Filtration Products

Separators and coalescers

In-line or offset piping

Single and two-stage

Exhaust heads

Float drain traps

Internal installations

Gas/Liquid Separators

Smart technology for cleaner, dryer air, gas, and steam



Guide to Eaton Gas/Liquid Separators

Removes up to 99% of all liquid and solid entrainment particles ≥ 10 µm

Special types also offer smaller retention rates



Eaton's application specialists are available to help every step of the way from initial selection through installation and start-up.

Steam

Eaton Gas/Liquid Separators installed ahead of steam turbines protect the turbine blades from the erosive action of wet steam, pipe scale and other damagecausing entrained solids. Installed in steam distribution lines, they assure clean, dry steam entering the heat exchangers, pressure reducing valves, temperature regulators, meters and other expensive process equipment.



Compressed air

An Eaton Gas/Liquid Separator installed following an intercooler or aftercooler removes entrained moisture, which would otherwise cause damage in successive stages of compression or to subsequent processes. Separators are often used to remove damage-causing entrainment in primary air lines leading to such equipment as air chucks, air nozzles and paint spray equipment. They are perfect for long runs of pipe and where wide temperature differentials are found. The separators are also very efficient in moisture separation of refrigerated air dryer packages.

Compressed gas

Eaton Gas/Liquid Separators installed in conjunction with intercooler and aftercooler equipment are especially efficient in the removal of oil, tar, water and other damagecausing entrainment.



Unique vortex containment plate (VCP) improves separator efficiency—only from Eaton

Ordinary separators often operate at less than peak efficiency due to the re-entrainment of separated liquid at normal and high-end flow rates. Eaton's unique vortex containment plate prevents, that already separated liquid and particles, even at high flow rates, cannot be entrained again by the gas flow. The VCP is made up of carefully placed rings that shield the separated liquid from the vortex action inside the separator and also directs the liquid to the separator drain. The turbulence of the swirling gas or air flow is sheltered from the liquid and cannot be re-entrained after separation. This prevents recontamination after separation. The VCP features extremely heavy-duty construction and is virtually maintenance free.



Choose the best Eaton Gas/Liquid Separator for any application

Туре Т

The popular choice for most applications



Type TS

For applications with greater than average liquid loading



Type TF and 31-LSF

Two-stage system separates liquid particles larger than 0.3 μm



Type R

Handles applications with liquid slugs



Type CLC

Removes entrainment down to 4 microns, twice as efficient as other separators



Type L

Ten different piping configurations fit most applications



Type DTL

For applications with greater than average solids loading



Type I

Can be installed into receivers, steam drums or other vessels



Type 40

Removes water and oil from exhaust gases, reduces roof maintenance and saves boiler condensate



Type AC/ACN

Float drain tap designed especially for separators; all stainless steel internals



Air Flow Capacity Chart

The values on the chart represent maximum recommended air flow in standard cubic feet per minute through standard separators.

The chart is based on SCFM (cubic feet per minute of air measured at standard conditions of 0 psi and 60° F). If any of the operating conditions are varied from these, consult Eaton.



Saturated Steam Flow Capacity Chart

The values on the chart represent maximum recommended saturated steam flow in pounds per hour through standard separators.

The chart is based on SCFM (cubic feet per minute of air measured at standard conditions of 0 psi and 60°F). If any of the operating conditions are varied from these, consult Eaton.



 $1 \text{ SCFM} = 1.7 \text{ m}^3/\text{h}$ 1 psi = 0.069 bar1 Pfund = 0.45 kg

Temperature Correction Factor

Temp. °F (°C)	Factor
-20 (-28.9)	0.904
-10 (-23.3)	0.917
0 (-17.8)	0.929
10 (-12.2)	0.941
20 (-6.7)	0.953
30 (-1.1)	0.965
40 (4.4)	0.977
50 (10.0)	0.989
60 (15.6)	1.000
70 (21.1)	1.012
80 (26.7)	1.023
90 (32.2)	1.034
95 (35.0)	1.040
100 (37.8)	1.046
105 (40.6)	1.051
110 (43.3)	1.057
120 (48.9)	1.068
130 (54.4)	1.079
140 (60.0)	1.090
150 (65.6)	1.101
160 (71.1)	1.112
170 (76.7)	1.121
180 (82.7)	1.133
190 (87.8)	1.143
200 (93.3)	1.154
250 (121.1)	1.206
300 (148.9)	1.256
400 (204.4)	1.353
500 (260.0)	1.445
550 (287.8)	1.490
600 (315.6)	1.533
700 (371.1)	1.618
800 (426.7)	1.701
900 (482.2)	1.780
1000 (537.8)	1.858

Specific Gravity Correction Factors

Gas	Symbol	M.W.	G	Fg
Hydrogen	H ₂	2.0	0.069	0.344
Helium	He	4.0	0.138	0.452
Synthesis	75% H ₂ 25% N ₂	8.5	0.295	0.611
Coke Oven	-	11.0	0.379	0.679
Methane*	CH ₄	16.0	0.551	0.788
Ammonia	NH ₃	17.0	0.586	0.808
Steam (Water Vapor)	H ₂ O	18.0	0.621	0.826
Natural Gas*	75% CH ₄ 25% N ₂	-	-	-
Acetylene	C_2H_2	26.0	0.897	0.957
Nitrogen	N ₂	28.0	0.950	0.986
Carbon Monoxide	CO	28.0	0.950	0.986
Air	-	29.0	1.00	1.00
Flue Gas	$81\% N_2 19\% CO_2$	31.0	1.08	1.027
Oxygen	02	32.0	1.10	1.039
Argon	А	39.9	1.38	1.136
Propane	$C_{3}H_{8}$	44.1	1.52	1.182
Carbon Dioxide*	CO ₂	44.0	1.52	1.181
Nitrous Oxide	N ₂ 0	44.0	1.52	1.181
Butadiene	$C_4 H_6$	54.1	1.86	1.284
Sulfur Dioxide	SO ₂	64.1	2.21	1.374
Chlorine	Cl ₂	70.9	2.45	1.431
Freon 12	CCI ₂ F ₂	120.9	4.17	1.770

*For applications involving gases (above 34 bar at 93°C), contact Eaton to determine whether there is an additional correction factor for compressibility.

The Eaton Flow Charts on the previous pages are based on SCFM (cubic feet per minute of air measured at standard conditions of 0 psi and 60° F) or pounds of steam per hour. If any of the operating conditions are varied from the above, then correction factors must be applied.

To use the Air Flow Chart for applications involving other gases

or other than standard conditions, the following equation must be solved for Q_c :

$$Q_{c} = Q_{sa} \times F_{a} \times F_{f}$$

In the event that Qsg is not provided in the proper form, any of the following equations may be used to arrive at the correct flow rate to insert in the above equation:

Sym	bol K	e
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- F_g = Correction factor for specific gravity
 - F_t = Correction factor for temperature (See table on the inside page)
- G = Specific gravity
- MMSCFD = Million standard cubic feet per day
 - MW = Molecular weight
 - P_a = Pressure (psia) at which volume is measured
 - Q_a = Rate of flow-standard cubic feet per minute (ACFM)
 - Q_c = Rate of flowstandard cubic feet per minute of equivalent air
 - Q_{sg} = Rate of flowstandard cubic feet per minute
 - T = Operating temp. (°F/°C)
 - T_a = Temperature (°F/°C) at which volume is measured

W = Rate of flowpounds per hour

$Q_{sg} = \frac{6.3 \times W}{MW}$ $Q_{sg} = 35.7 \times Q_a \times P_a$

$$\frac{6677742}{460 + T_a}$$

 $O_{sg (air only)} = 0.218 \times W$

$$Q_{sg} = \frac{MMSCFD}{1440}$$

 $W = (pounds mols/hour) \times MW$

Application Data Sheet

Name:		Date	ə:			
Title:						
Company:						
Address:						
City:		State:		_ Zip:		
Phone:		Fax:				
E-Mail:						
Product(s) of Interes	t					
🗆 ТуреТ	🗆 Туре I	🗆 Туре	e R			
□ TypeTS	□ TypeTF	🗆 Туре	e DTL	□ Type 31-LSF		
🗆 Туре L	□ Type CLC	🗆 Туре	e 40	□ Type AC/ACN		
Application Paramet	ers					
Pipe Size:	_in	mm				
Flow Medium:	□ Steam	Natural Gas	□ Other			
Volumetric Flow:	SCFM	m³/h		Nm³/h		
Weight Flow:	kg/h					
Average Molecular Weigh	t:					
Minimum Operating Press	sure:	barg				
Maximum Operating Tem	perature:	°C				
Flow Configuration Preference: U Vertical Flow Horizontal Flow						
Design Pressure of Vessel	:I	barg				
Design Temperature of Ves	ssel:	°C				
Maximum Entrained Liqu	id:	_ kg/h				
End Connections Required	d: 🗆 Threa	aded 🗆 Flanged [□ Socket We	ld		
□ PN10 / 125# PN16 / 150# □ PN40 / 300# □ Other						
Materials of Construction: Cast Iron Carbon Steel Stainless Steel						
□ Other						

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